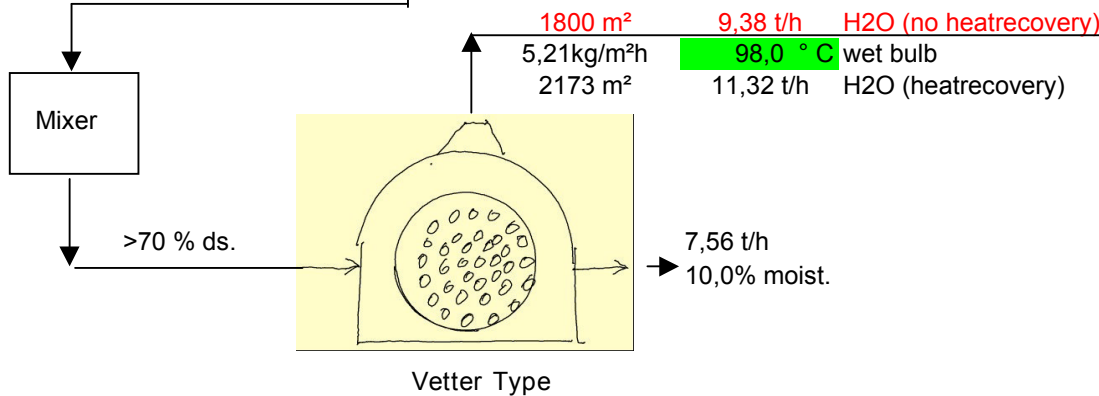


# Feed production from starch

Ethanol Production = Strg+e

Starch Production = Strg+s

- Rawmaterial 14 % moisture (corn or wheat)
- Total residues to feed of rawmaterial
- Solid residues to feed of total residues
- Soluble residues to feed of total residues
- Solid residues to dryer
- Soluble residues before evaporation
- Solubles residue after evaporation
- Solubles residue after evaporation



	heatrecovery	no heatrecovery
Liquid residues (to feed) % ds =	32,9%	45,0%
Nr. of evaporator stages	2	3
Stage evaporator efficiency	0,55	0,37
Steam to dryers (both systems equal)	10,0 bar absolut	179,9 ° C
Dryer condensate flash steam pressure	1,0 bar absolut	99,6 ° C
Fresh steam flow to dryers	15,0 t /h	12,4 t /h
Dryer condensate flash steam return	- 2,3 t /h	- 1,9 t /h
Evaporator steam demand	10,58 t /h	7,77 t /h
Steam for evap. obtained from heatrecovery	- 10,58 t /h	
<b>Total consumption (Standart steam 1 bar)</b>	<b>12,7 t /h</b>	<b>18,3 t /h</b>
fresh steam to evaporator (1 bar)	0,00 t/h	7,77 t /h fresh steam to evaporator (1 bar)

	1000 tcb/d
19,0%	6,8 ds t/h
65,0%	4,4 ds t/h
35,0%	2,4 ds t/h
38,0 % ds	11,6 t /h
9,0 % ds	26,5 t /h
32,9 % ds	7,2 t /h
45,0 % ds	5,3 t /h

